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## Revisions to Original Claims

- A comprehensive [NG] gas processor for removing the moisture and recovering the higher hydrocarbons (i.e., C<sub>2</sub><sup>+</sup>) therein either on-situ in a gas field or in a plant comprising:
  - (a) an integrated [NG] gas processor adopting comprising two sections working on a hybrid process, i.e., an integration of two different processes within a single casing:
    - i) a refrigeration-dehydration section working on refrigeration process wherein the inlet gas contacts with a counter-flowing stream of dispersed cold heat-transport medium containing a non- or low-volatile hydrate inhibitor with boiling point higher than 180°C and the moisture of said gas is condensed and removed with the cold heat-transport medium; and
    - ii) an absorption section working on low-temperature absorption process wherein the dehydrated gas contacts with a counter-flowing stream of dispersed liquid absorbent with a hydrocarbon gas solubility higher than 20 scf/gal wherein the higher hydrocarbons (i.e., C<sub>2</sub><sup>+</sup>) are absorbed.

[and connected to the raw NG inlet pipeline and the lean NG outlet pipeline;]

- (b) a heat-transport medium cooler [connected to the medium inlet and transfer pipelines;]

  comprising a pre-cooling stage and a deep-cooling stage wherein in said pre-cooling

  stage said heat-transport medium is pre-cooled with the cold outlet gas left said

  integrated gas processor and in said deep-cooling stage the medium is deep-cooled with

  the refrigerant provided with a refrigerator;
- (c) an absorbent cooler [connected to the absorbent inlet and recycle pipelines;] comprising a pre-cooling stage and a deep-cooling stage wherein in said pre-cooling stage said recycling absorbent is pre-cooled with the cold outlet absorbent left said integrated gas processor and in said deep-cooling stage the absorbent is deep-cooled with the refrigerant provided with a refrigerator;
- (d) a fractional distiller [connected to the rich oil transfer and outlet pipelines, the absorbent outlet pipeline, and the product outlet pipeline.] for separating the absorbed higher hydrocarbons as a product from the outlet absorbent left said integrated gas processor



- and then the [latter] separated absorbent is recycled back to said integrated gas processor;
- (e) an inhibitor regenerator [connected to the effluent transfer pipeline, the inhibitor recycle pipeline and the wastewater discharge pipeline;] for concentrating the low-volatile hydrate inhibitor to be recycled and discharging the wastewater;
- (f) a [refrigeration unit connected to the refrigerant inlet and outlet pipelines] refrigerator for providing the refrigerant to said deep-cooling stages of said heat-transport medium cooler and said absorbent cooler;
- (g) a pipeline for delivering the recovered higher hydrocarbons; and
- (h) a gas inlet pipeline and a pipeline for delivering the [lean NG] processed gas.
- 2. A comprehensive [NG] gas processor of claim 1 wherein the dehydration section of said integrated processor and its accessories (comprising said heat-transport medium cooler, said inhibitor regenerator, said refrigerator, and said gas inlet pipeline and a pipeline for delivering the processed gas) are operated independently as a [pure NG] gas dehydrator without incorporating the absorption section.
- 3. A comprehensive [NG] gas processor of claim 1 wherein [a] said heat-transport medium is [in directly contact with the counter-flowing NG in the dehydration section] an aqueous solution of calcium chloride or other ionizing salts and the regeneration rate of said solution is less than 5 liter per kg of wastewater to be discharged.
- 4. A comprehensive gas processor of claim 1 wherein said heat-transport medium is an aqueous solution of ethylene glycol or other organic compounds with boiling points higher than 180°C and the regeneration rate of said solution is less than 5 liter per kg of wastewater to be discharged.
- 5. A comprehensive [NG] gas processor of claim 1 wherein [an] said absorbent is [in directly contact with the counter-flowing NG in the absorption section] heavy oil (i.e., hydrocarbon mixture with molecular weight higher than 100) or other organic compounds with hydrocarbon gas solubility higher than 10 scf/gal liquid.
- [5. A comprehensive NG processor of claim 1 wherein the heat-transport medium contains a



gas-hydrate inhibitor.]

[6.A comprehensive NG processor of claim 1 wherein the refrigeration unit is an industrial refrigerator.]

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- 6. A comprehensive [NG] gas processor of claim 1 when working on inlet gas pressure greater than 5.0 MPa wherein [the refrigeration unit] said refrigerant to said deep-cooling stages of said heat-transport medium cooler and said absorbent cooler is provided with a [NG] gas expansion device.
- [8. A comprehensive NG processor of claim 7 wherein a gas-hydrate inhibitor is injected into the NG before entering the NG expansion device.]
- [9.A comprehensive NG processor of claim 7 wherein the NG expansion device is a gas expansion valve.]
- [10.A comprehensive NG processor of claim 7 wherein the NG expansion device is a turbo expander-compressor.]

[11.]

A [comprehensive NG processor] gas expansion device of claim [7] 6 wherein [the NG] said expansion [equipment] device is a triple-sectional free-piston [NG] gas expander-compressor\_booster comprising:

- (a) [A]a gas expansion cylinder and a gas compression cylinder;
- (b) [A]a co-shaft gas expansion piston and gas compression piston; and
- (c) a co-shaft gas-fueled booster piston engine providing supplemental power for compressing said expanded gas to the required delivery pipeline pressure.

In JM 12/16/2002